

Fixed Orifice Double Regulating Globe Valve with Isolation Ball Valve

Feature

- DZR brass fixed orifice double regulating globe valve
- Venturi insert
- Positive shut-off with memory stop
- Design according to BS7350
- Tolerance on nominal Cvs $\pm 3\%$ (test according to BS7350)
- Multi-turn adjustment (four full turns minimum)
- Union ends (ASME B1.20.1 - NPSM) for tailpiece connections
- FNPT, MNPT, Solder, EzPress and PEX (F1960) tailpieces available
- Isolation ball valve with union nut for ON/OFF operation
- FNPT, Solder, EzPress and PEX (F1960) available for ball valve
- Blow-out proof stem, adjustable packing



Meet BAA requirement

300WOG

Working conditions:

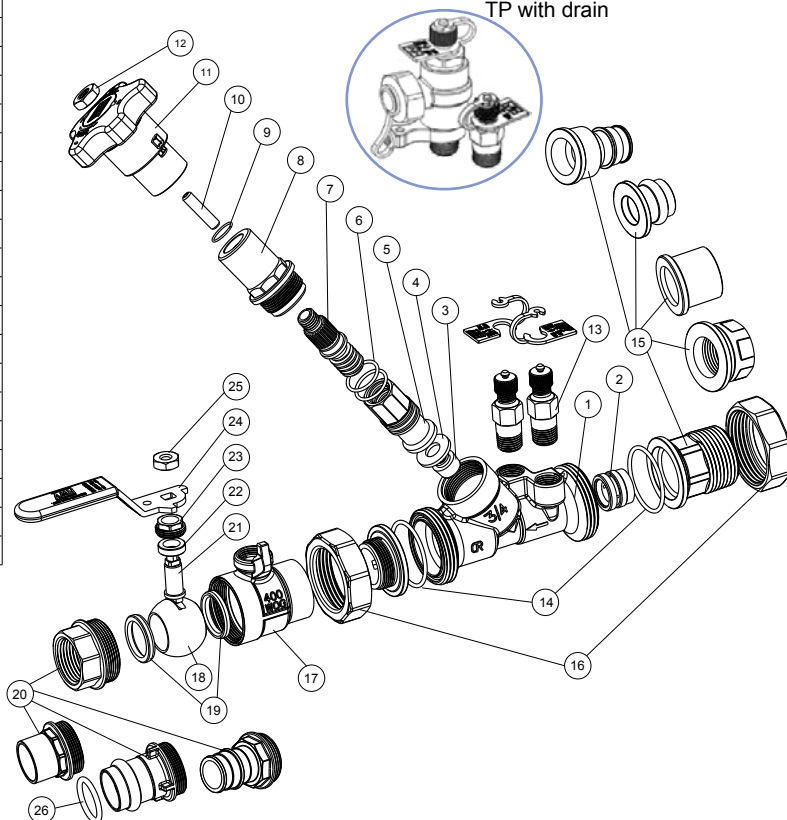
- Water: from 15°F to 260°F
- below 32°F only for water with added antifreezing fluids
- over 212°F only for water with added anti-boiling fluids

Material

Part	Material	Specification
1	Body	DZR Brass UNS C35330
2	Venturi insert	DZR Brass UNS C35330
3	Balancing cone	DZR Brass UNS C35330
4	Gasket disc	PTFE
5	Shutter	DZR Brass UNS C35330
6	Disc O-ring	EPDM Perox
7	Disc stem	DZR Brass UNS C35330
8	Bonnet	DZR Brass UNS C35330
9	Stop spring ring	Spring steel
10	Stem	Brass
11	Handwheel	ABS (blue)
12	Nut	Steel / Zn plated
13	Test point	DZR Brass ¹
14	Union O-ring	EPDM Perox
15	Tailpiece ²	DZR Brass
16	Union nut	Brass
17	Body	DZR Brass UNS C35330
18	Ball	DZR Brass / Cr plated
19	Seat	PTFE
20	Fixed end	DZR Brass UNS C35330
21	Stem	DZR Brass UNS C35330
22	Packing ring	PTFE
23	Packing nut	Brass
24	Handle	Steel / Dc plated
25	Nut	Steel / Dc plated
26	O-ring	EPDM Perox

¹ Test points with EPDM Perox gaskets and polypropylene ties
² Any possible combination of tailpiece available

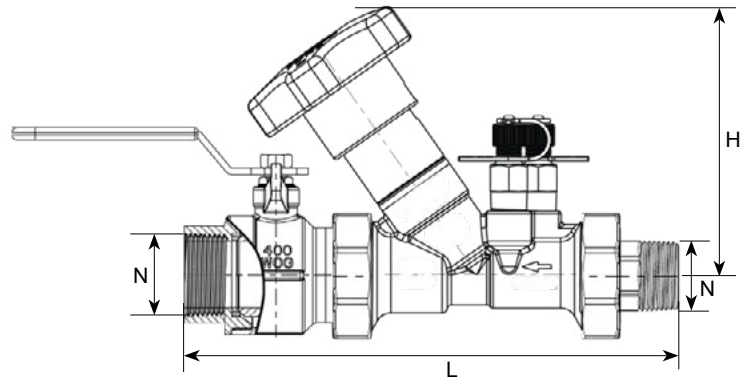
Optional:
Fig. 95TP-SD
High pressure
TP with drain



Dimension, Weight

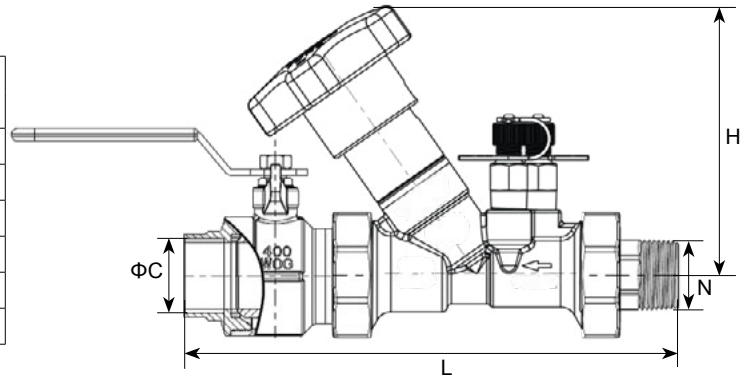
9517IBV-MF

Size	N	H [in]	L [in]	Weight [lb]	Flow range [GPM]
X-1/2"	1/2 - 14 NPT	4.06	6.77	2.08	0.12-0.36
U-1/2"	1/2 - 14 NPT	4.06	6.77	2.08	0.27-0.71
L-1/2"	1/2 - 14 NPT	4.06	6.77	2.08	0.49-1.17
1/2"	1/2 - 14 NPT	4.06	6.77	2.08	0.98-2.35 ¹
3/4"	3/4 - 14 NPT	4.06	7.28	2.81	2.19-5.15 ¹
1"	1 - 11.5 NPT	4.06	8.08	3.39	4.09-9.56 ¹



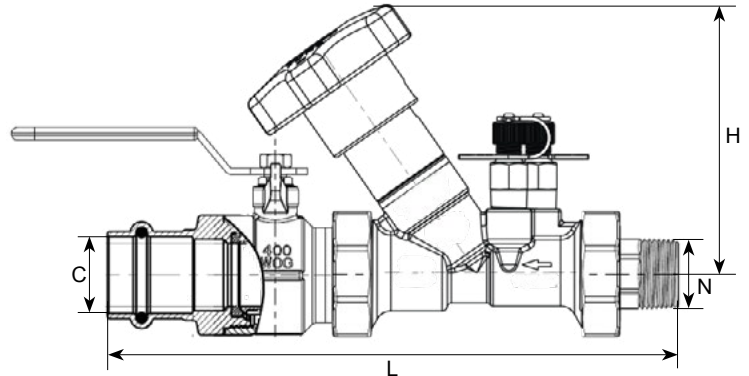
9517IBV-MS

Size	N	ΦC ² [in]	H [in]	L [in]	Weight [lb]	Flow range [GPM]
X-1/2"	1/2 - 14 NPT	0.627-0.631	4.06	5.34	1.63	0.12-0.36
U-1/2"	1/2 - 14 NPT	0.627-0.631	4.06	5.34	1.63	0.27-0.71
L-1/2"	1/2 - 14 NPT	0.627-0.631	4.06	5.34	1.63	0.49-1.17
1/2"	1/2 - 14 NPT	0.627-0.631	4.06	5.34	1.63	0.98-2.35 ¹
3/4"	3/4 - 14 NPT	0.877-0.881	4.06	5.78	1.94	2.19-5.15 ¹
1"	1 - 11.5 NPT	1.128-1.131	4.06	6.66	2.49	4.09-9.56 ¹



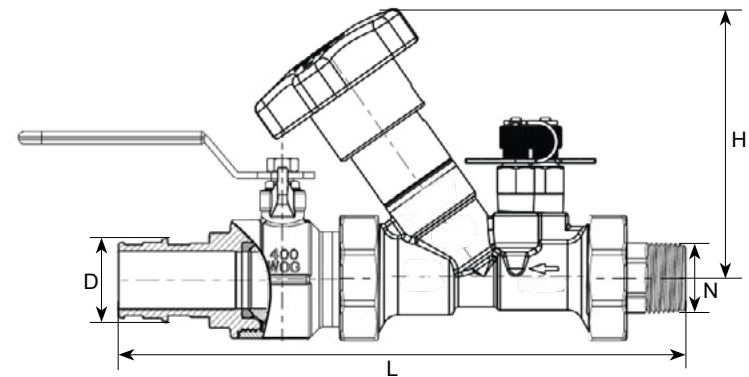
9517IBV-MP

Size	N	C [in]	H [in]	L [in]	Weight [lb]	Flow range [GPM]
X-1/2"	1/2 - 14 NPT	0.64	4.06	7.27	1.99	0.12-0.36
U-1/2"	1/2 - 14 NPT	0.64	4.06	7.27	1.99	0.27-0.71
L-1/2"	1/2 - 14 NPT	0.64	4.06	7.27	1.99	0.49-1.17
1/2"	1/2 - 14 NPT	0.64	4.06	7.27	1.99	0.98-2.35 ¹
3/4"	3/4 - 14 NPT	0.89	4.06	8.05	2.46	2.19-5.15 ¹
1"	1 - 11.5 NPT	1.14	4.06	9.03	3.26	4.09-9.56 ¹



9517IBV-ME

Size	N	D [in]	H [in]	L [in]	Weight [lb]	Flow range [GPM]
X-1/2"	1/2 - 14 NPT	1/2" F1960	4.06	7.02	1.88	0.12-0.36
U-1/2"	1/2 - 14 NPT	1/2" F1960	4.06	7.02	1.88	0.27-0.71
L-1/2"	1/2 - 14 NPT	1/2" F1960	4.06	7.02	1.88	0.49-1.17
1/2"	1/2 - 14 NPT	1/2" F1960	4.06	7.02	1.88	0.98-2.35 ¹
3/4"	3/4 - 14 NPT	3/4" F1960	4.06	7.78	2.37	2.19-5.15 ¹
1"	1 - 11.5 NPT	1" F1960	4.06	8.77	3.06	4.09-9.56 ¹



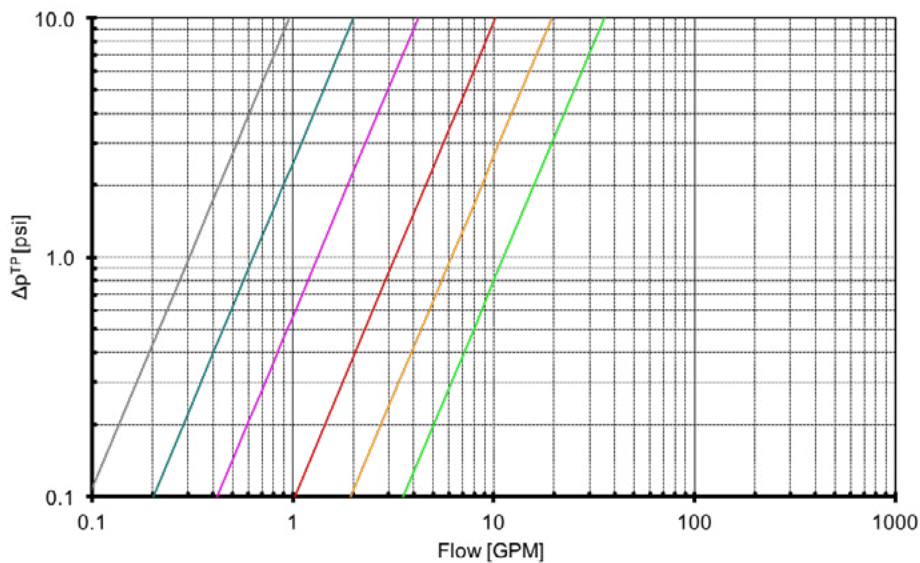
¹ Suggested flow range applicability (BS7350)

² Tolerance field

If using a measuring manometer different from those proposed by RWV please verify that sensibility of the measuring device is compatible with indicated minimum flow (see flow measurement paragraph)

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Flow Measurement



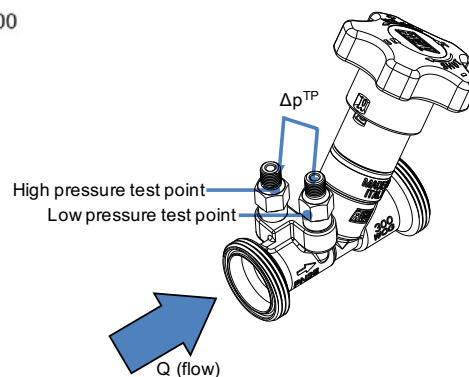
X-1/2"	Cvs venturi 0.304
U-1/2"	Cvs venturi 0.64
L-1/2"	Cvs venturi 1.33
1/2"	Cvs venturi 3.24
3/4"	Cvs venturi 6.16
1"	Cvs venturi 11.24

Q = flow rate in GPM

Δp = differential pressure signal generated through pressure test points

Cv = flow coefficient

$$Q = C_{vs}^{venturi} \cdot \sqrt{\Delta p^{TP}}$$



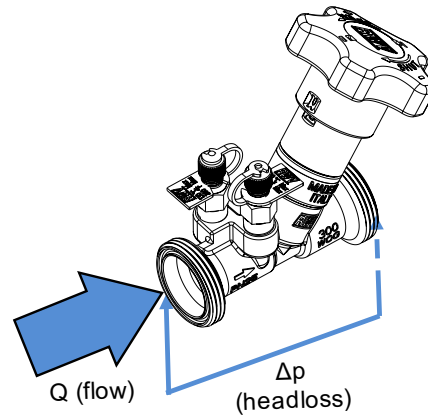
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Headloss

Handwheel position	Cv (GPM/psi ^{0.5})					
	X-1/2"	U-1/2"	L-1/2"	1/2"	3/4"	1"
0.5	0.061	0.177	0.160	0.474	0.47	1.70
0.7	0.072	0.206	0.186	0.474	0.54	2.00
1.0	0.124	0.283	0.287	0.613	0.67	2.42
1.3	0.169	0.331	0.394	0.717	0.81	2.82
1.5	0.193	0.355	0.440	0.809	0.90	3.12
1.7	0.217	0.387	0.501	0.902	0.99	3.48
2.0	0.250	0.445	0.586	0.99	1.12	4.13
2.3	0.267	0.511	0.67	1.10	1.25	4.83
2.5	0.274	0.517	0.70	1.18	1.39	5.28
2.7	0.280	0.527	0.74	1.32	1.62	5.63
3.0	0.291	0.563	0.83	1.60	2.24	6.09
3.3	0.294	0.578	0.86	1.88	2.94	6.49
3.5	0.299	0.594	0.89	2.03	3.39	6.64
3.7	0.302	0.595	0.92	2.12	3.75	6.80
4.0	0.303	0.603	0.95	2.19	4.06	7.10
4.4	0.305	0.605	0.98	2.22	4.24	7.21

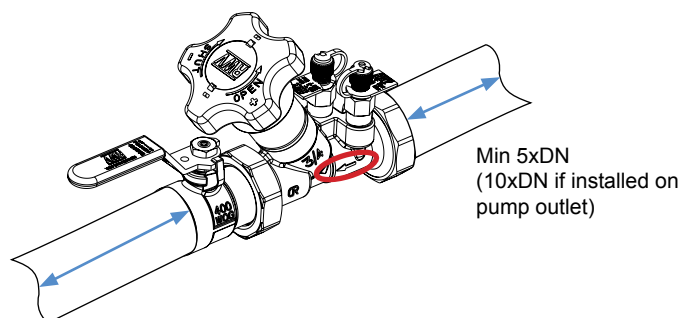
Formula linking flow Q (in GPM) and theoretical valve headloss Δp (in psi). Cv depends on handwheel position as indicated on table.

$$\Delta p = \left(\frac{Q}{C_v} \right)^2$$



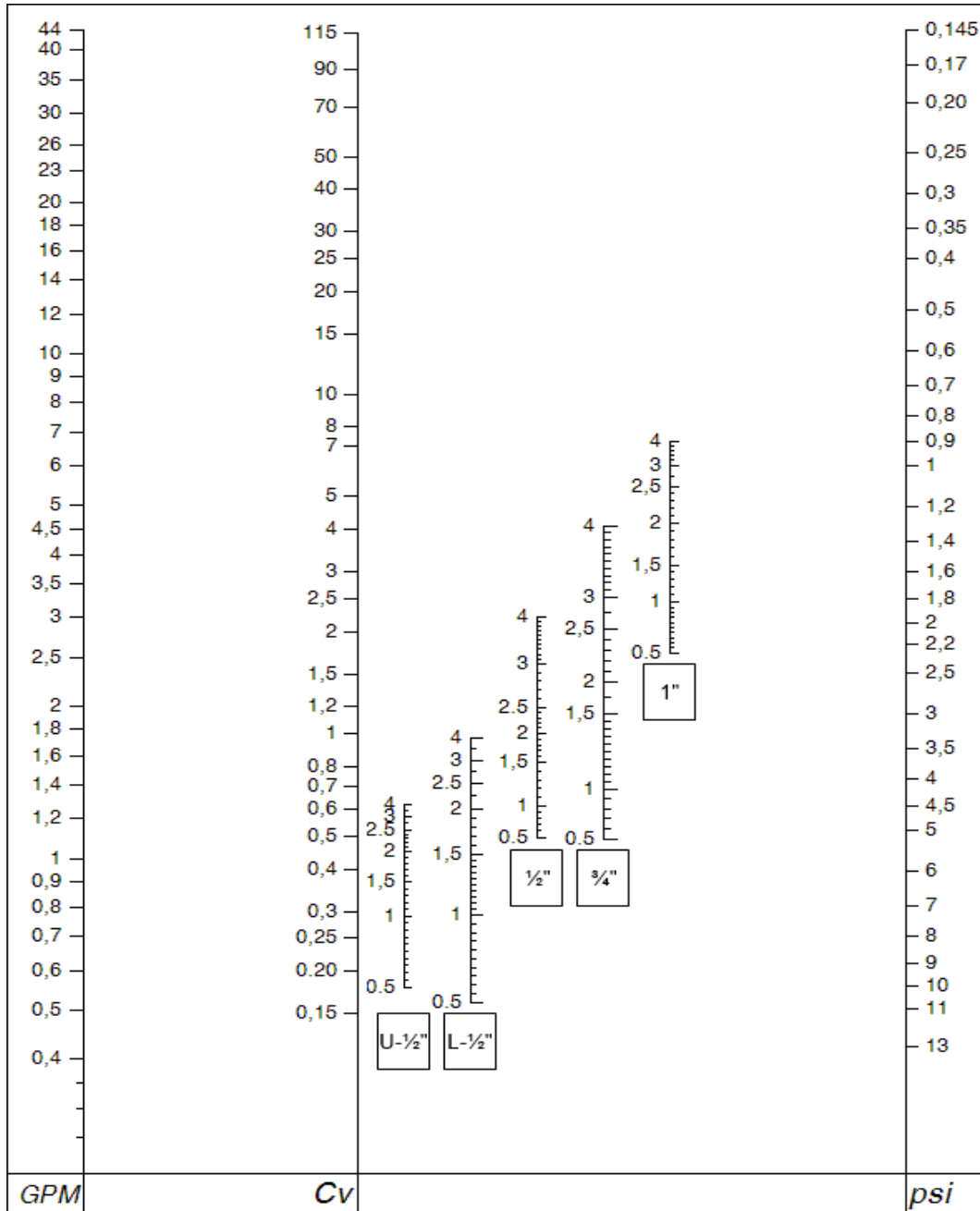
Installation

To obtain the best performances valve must be installed on a pipe with its same nominal size preceded by straight pipe lengths as per figure indications.



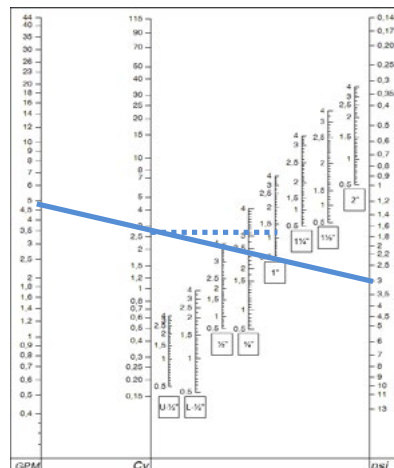
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Presetting



Using the diagram above, it is possible to determine the presetting position of the valve with the given design flowrate and headloss:

- 1) draw a straight line joining design flowrate and design headloss;
- 2) determine design Cv value as intersection of drawn line and Cv axis;
- 3) draw a straight horizontal line from intersection previously identified and the specific valve size Axis;
- 4) intersection determines handwheel position to use for presetting.



In the example for a design flowrate of 5GPM and design Δp 3psi handwheel position of 1.35 is determined for a 1" valve